

Technologies for Pollution Control

Ozonation

KEYWORDS: Ozonation / Membranes for O₃/O₂ Separation / NETmix / Membrane Contactor / Water Treatment

New ozone (O₃)-technology solutions, offering means to its wider implementation by providing innovative cost-effective systems, including (i) customized membranes for the separation of O₃/oxygen (O₂) gas stream from the O₃ generator, enabling the recycling of the O₂ enriched gas stream back to the O₃ generator; (ii) low footprint O₃ side stream contacting train, integrating the static mixer NETmix or membrane contactor, able to enhance the O₃ mass transfer from the gas phase to the liquid phase.

Introduction

The increasing global health concerns due to the surge in urbanization, increasing water contamination, and increasing world industrialization are driving the ozone (O₃) technology market globally.

O₃ is usually produced by passing a stream of O₂ through a corona discharge system, which provides energy to convert O₂ to O₃. The reactive nature of O₃ typically limits the capability of O₃ generators to produce O₃ in concentrations greater than 15%, resulting in low yield and high O₃ production costs. High O₃ supply demands, the extended contacting time required in the reaction chamber, and the bulky size of the equipment (low gas-liquid mass transfer rates of O₃) also constitute a major impediment to the mass penetration of O₃ technology in the water treatment sector.

Our goal is to address these issues by developing disruptive O₃ technology for water treatment, including: (i) functionalized membranes for O₃/O₂ separation to obtain an O₃-enriched gas stream, enabling an O₃ generation at lower concentration while utilizing less specific power; simultaneously, the O₂ from the mixture of O₂/O₃ can be recovered and recycled back to the O₃ generator, thereby saving costs for the energy to produce O₂ and reduce the O₂ consumption; and (ii) the development of a low footprint O₃ side stream contacting train for water treatment; the integration of the O₃/O₂ separation unit with a pressurized static micro/meso-structured mixer (NETmix) or membrane contactor, enhancing the O₃ mass transfer from the gas phase to the liquid phase to 100% or very close to it, thus leading to an enriched water stream and resulting in a downstream highly compact reaction chamber.

This project brings together different academia (FEUP) and industry (SIMBIENTE, Enkrott, and AdP Valor) researchers with complementary competencies and expertise.

Current Development

Under the OZONE4WATER project (www.ozone4water.com), a gas separation setup was designed and constructed (Fig 1), comprising the following main components: (i) corona discharge O₃ generator; (ii) diaphragm pump to compress the O₃ stream; (iii) membrane modules (flat sheet or spiral-wound), incorporating the synthesized membranes; and (iv) O₃ analyzer. Various membranes with customized properties for O₂/O₃ separation are being prepared and tested, including functionalized asymmetric PVDF/PDMS flat membranes and a commercial symmetric PDMS spiral-wound membrane.

Mathematic models for the O₃/O₂ separation in two different membrane configurations and for the flow patterns that may appear in each one of the membranes (cross-flow in the SWM, and co-current, counter-current, and cross-flow in the HF membranes) were studied, allowing a better

understanding of the influence of the different parameters on the efficiency of the separation. The overall analysis showed that, regardless of the membrane geometry, the effect of each parameter in the membrane performance is similar, i.e., it promotes the variation of the permeate composition in the same direction. The O₃/O₂ separation was also evaluated experimentally in the PDMS spiral wound membrane, resulting in O₃/O₂ selectivity of 1.3 %.

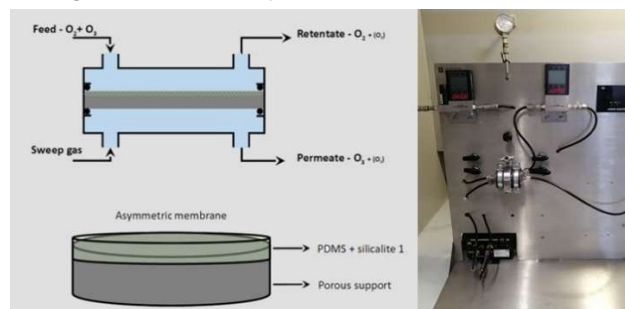


Fig 1. Scheme of flat module membrane and asymmetric membrane (left), and photograph of the gas separation setup (right).

The O₃ dissolution in the NETmix, as a function of reactor design parameters and operating conditions, was determined experimentally and validated by co compute fluid dynamics (CFD) modeling. Fig 2 shows the volumetric mass transfer coefficients ($k_L a$) and energy consumption per mass of injected liquid (P/M) associated with a NETmix unit containing 8 columns and 29 rows of unit cells in an air-water system. The NETmix technology exhibits a high gas-liquid transfer performance whilst maintaining a low energy consumption when compared to other typical commercially available static mixers.

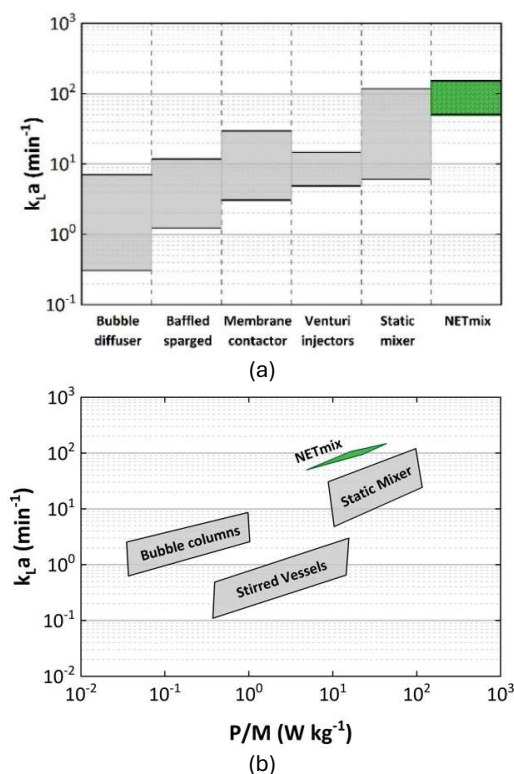
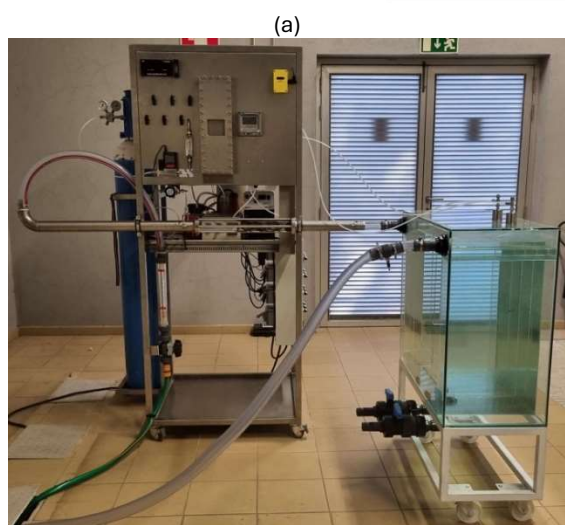
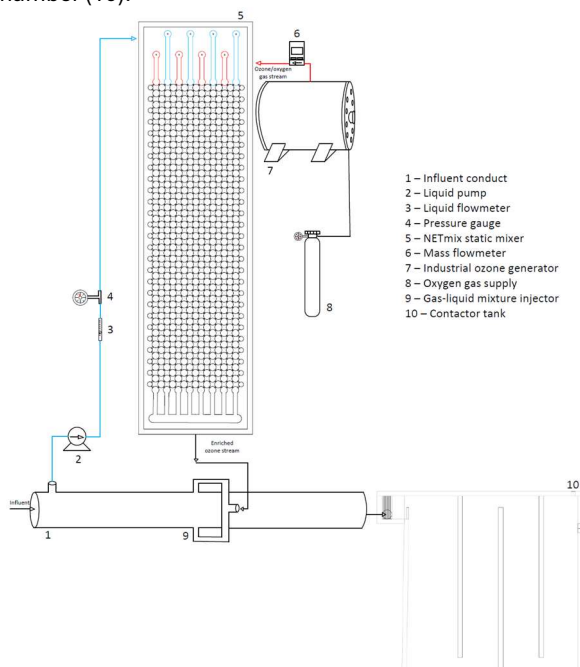


Fig 2. Measured $k_L a$ values (a) and P/M associated with the NETmix (b), in comparison with other technologies.

Based on CFD modeling, a new NETmix unit was designed and constructed comprising two innovative injection cones for the separate distribution of the entrance fluids at the mixer's inlet: each cone has a circular entrance and an elliptical base. Therefore, both liquid and gas phases are injected separately into four cylindrical chambers. Hence, the two phases interact solely at the micro/meso-structured network of unit cells characteristic of the NETmix technology. At the outlet, the exiting gas-liquid mixture is collected by an identical cone.

A prototype for water treatment using an O₃ side stream contacting train was designed and constructed (Fig 3). A portion of the main water flow (1) is split off into a side stream. Compressed O₃ gas and water (side stream) are injected in the NETmix pressurized reactor (1-5 bar), boosting O₃ dissolution. The supersaturated O₃-enriched water stream leaves the NETmix and is rapidly blended into the main water flow (9), providing the stable dissolved O₃ required to obtain the oxidation/disinfection credits in the contact/reaction chamber (10).



(b)

Fig 3. Scheme (a) and photograph (b) of the prototype.

Under the NOR-WATER project, a membrane O₃ contactor, operated under continuous mode, was developed and tested for the tertiary treatment of urban wastewater (UWW), targeting the removal of contaminants of emerging concern (CECs), bacterial disinfection, and toxicity reduction. This system relies on the homogeneous radial distribution of O₃ in the reaction zone by "titration" through a microfiltration tubular membrane, while the UWW swirls around the membrane and drags the O₃ microbubbles generated in the membrane shell-side. The ozonation tests were carried out with secondary-treated UWW collected in different seasons (winter and summer) and spiked with a mix of 19 CECs (10 µg L⁻¹ each). For an O₃ dose of 18 g m⁻³, removals above 80% or concentrations below the limit of quantification were obtained for up to 13 of the 19 CECs and reductions up to 5 log units for total heterotrophs and below the limit of detection for enterobacteria and enterococci. After ozonation, the abundance of antibiotic-resistant bacteria was reduced but not eliminated, and microbial regrowth after 3-day storage was observed. No toxic effect was detected on zebrafish embryos using a dilution factor of 4 for the ozonized UWW, and when granular activated carbon adsorption was subsequently applied, the dilution factor decreased to 2.

Future Perspectives

OZONE4WATER project: Validation of the ozonation prototype for the pre-oxidation of freshwater and tertiary treatment of urban wastewater, thereby allowing for access to safe and affordable drinking water and production of irrigation-grade treated urban wastewater, safe for reuse in agriculture; Environmental, economic, and social impacts of the technology.

NEWater project, supported by the Water4All program: Integration of ozonation, biofiltration, and membrane filtration for the treatment of secondary municipal wastewater, enabling the production of a high-quality permeate for electrolysis.

Related Sustainable Development Goals



Outputs

PhD Theses

[1] Pedro Henrique Presumido, Membrane processes for tertiary treatment of urban wastewaters: photocatalytic membrane reactor and ozone membrane reactor, PDEA, FEUP, 2023

Master Dissertations

[1] Cristiana Andreia Vieira Gomes, Intensification of ozonation processes for water treatment: ozone/oxygen separation by membrane, MIEQ, FEUP, 2019

[2] Paulo Henrique Marrocos de Oliveira, A low footprint ozone mixer based on the NETmix technology: CFD modelling and experimental validation, MIEQ, FEUP, 2021

Selected Publications

[1] P.H. Presumido et al., J. Environ. Chem. Eng. 10, 108671 (2022)

[2] P.H. Presumido et al., Sci. Total. Environ. 892, 164492 (2023)

[3] M.M. Pituco et al., Chem. Eng. Process.: Process Intensif. 194, 109566 (2023)

Team

Vitor Vilar Principal Researcher; **Alexandre F.** Professor; **Ricardo J.** Auxiliar Researcher; **Madalena M.** Professor; **Rui Boaventura** Principal Researcher; **Francisca Moreira Junior** Researcher; **Pedro Presumido**, PhD Student; **Mateus Pituco**, PhD Student; **Mateus Caixeta**, PhD Student; **Paulo Marrocos**, PhD Student; **Inês Rodrigues**, PhD Student; **Cristiana Gomes**, PhD Student; **Laura Cullen**, Project Researcher

Funding

OZONE4WATER, PTDC/EAM-AMB/4702/2020, 2021-2024

NOR-WATER, 0725_NOR_WATER_1_P, 2019-2022

LSRE-LCM Base Funding, UIDB/50020/2020, 2020-2023

LSRE-LCM Programmatic Funding, UIDP/50020/2020, 2020-2023

LA LSRE-LCM Funding, UID/EQU/50020/2019, 2019

LA LSRE-LCM Funding, POCI-01-0145-FEDER-006984,2013-2018

FCT Grants: CEECIND/02196/2017, CEECIND/01317/2017

FCT Scholarships: SFRH/BD/138756/2018, SFRH/BD7144673/2019,

2020.06681.BD, 2022.10784.BD, 2022.10437.BD, 2021.05666.BD